arise from the different constraints imposed on the system, so that only experimental data can help in selecting the true Saha equation. Moreover, also accepting the maximization entropy criterion, we can have different formulations of the Saha equation depending on the definition of the relevant excitation temperatures, and these depend on the role of electrons and heavy particles in the dissociation and ionization processes.^{23–27}

Conclusions

We have presented new calculations of thermodynamic and transport properties of equilibrium and nonequilibrium H_2 plasmas. In general, our results are in good agreement with those obtained by other authors. 16,21,22 The main conclusion that can be drawn from the results is that the thermodynamic and transport properties of two-temperature plasmas may depend in a nonnegligible manner on the adopted form of the Saha equation, which, in turn, is determined by the physical constraints imposed on the considered system.

Acknowledgment

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Extended Slip Boundary Conditions for Microscale Heat Transfer

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Nomenclature

Kn = Knudsen number T = temperature, K u_s = slip velocity, m/s y = coordinate axis

Introduction

THE commonly used slip boundary conditions in microchannels are called the Maxwellian conditions, and they are first-order accurate in Knudsen number. In the present analysis, we develop the extended slip boundary conditions in a systematic manner to be used beyond the slip flow regime. The results are valid for early transition flows.

Analysis

A. Velocity Slip

When a gas flows over a surface, the molecules leave some of their momentum and create the shear stress on the wall. This momentum is the difference between the momentum of the incoming, $M_{\rm in}$, and the reflected, $M_{\rm out}$, molecules. The incoming momentum has two components: momentum of the impinging and the slipping molecules. The momentum going away from the surface is by reflection. As shown in Fig. 1, the specular reflection conserves the tangential momentum of the molecules $M_{\rm specular} = M_{\rm in}$, and the diffuse

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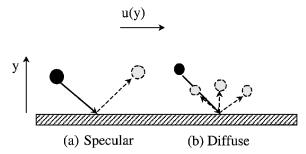


Fig. 1 Molecular reflection at the boundary.

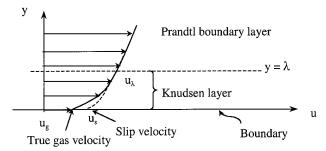


Fig. 2 Schematic of the velocity profile.

reflection results in vanishing tangential momentum, $M_{\rm diffuse}=0$. The fraction of the molecules that are diffusely reflected by the wall is defined as the tangential momentum accommodation coefficient F_m . When these definitions are used, the momentum leaving the surface can be written as

$$M_{\text{out}} = (1 - F_m)M_{\text{in}} \tag{1}$$

This results in the following wall momentum balance:

$$M_{\text{wall}} = F_m M_{\text{in}} \tag{2}$$

where the shear stress at the wall is given by $M_{\rm wall} = \mu ({\rm d} u/{\rm d} y)_0$ and the incoming momentum is given by $M_{\rm in} = \frac{1}{2} \mu ({\rm d} u/{\rm d} y)_0 + \frac{1}{2} \rho u_m u_0$. The first term is the momentum brought by the incoming stream, and the second term is due to the slip motion. Figure 2 shows the Knudsen layer next to the boundary. We will evaluate Eq. (2) at this layer thickness λ as

$$\mu \left(\frac{\mathrm{d}u}{\mathrm{d}y}\right)_{\lambda} = F_m \left[\frac{1}{2}\mu \left(\frac{\mathrm{d}u}{\mathrm{d}y}\right)_{\lambda} + \frac{1}{2}\rho u_m u_{\lambda}\right] \tag{3}$$

Equation (3) is solved for the velocity at $y = \lambda$ as

$$u_{\lambda} = \frac{2 - F_m}{F_m} \lambda \left(\frac{\mathrm{d}u}{\mathrm{d}y}\right)_{\lambda} \tag{4}$$

where λ is the molecular mean free path and is defined as $\lambda = 2\mu/\rho u_m$, where μ is the dynamic viscosity, ρ is the density, and u_m is the mean velocity.

Maxwell's slip boundary condition has been applied routinely in the slip flow regime and has generated satisfactory results. A However, as Knudsen number Kn increases, the results of this boundary condition deviate from the Boltzmann solution. We propose the following representation of the velocity gradient at the wall. This approach is different from Beskok and Karniadakis's approach in which they expanded the velocity at $y = \lambda$ around the wall instead of the velocity gradient. Therefore, we call the proposed relation the stress boundary condition and Beskok and Karniadakis's approach the velocity boundary condition.

The velocity gradient at $y = \lambda$ is expanded around y = 0 as

$$\left(\frac{\mathrm{d}u}{\mathrm{d}y}\right)_{\lambda} = \left(\frac{\mathrm{d}u}{\mathrm{d}y}\right)_{0} + \lambda \left(\frac{\mathrm{d}^{2}u}{\mathrm{d}y^{2}}\right)_{0} + \frac{\lambda^{2}}{2} \left(\frac{\mathrm{d}^{3}u}{\mathrm{d}y^{3}}\right)_{0} + \frac{\lambda^{3}}{6} \left(\frac{\mathrm{d}^{4}u}{\mathrm{d}y^{4}}\right)_{0} + \cdots$$

Substituting Eq. (5) into Eq. (4) yields

$$u_{s} = \frac{2 - F_{m}}{F_{m}} \lambda \left[\left(\frac{\mathrm{d}u}{\mathrm{d}y} \right)_{0} + \lambda \left(\frac{\mathrm{d}^{2}u}{\mathrm{d}y^{2}} \right)_{0} + \frac{\lambda^{2}}{2} \left(\frac{\mathrm{d}^{3}u}{\mathrm{d}y^{3}} \right)_{0} + \frac{\lambda^{3}}{6} \left(\frac{\mathrm{d}^{4}u}{\mathrm{d}y^{4}} \right)_{0} + \cdots \right]$$

$$(6)$$

Equation (6) is nondimensionalized by $u^* = u/u_m$, $\eta = y/\ell$, and $Kn = \lambda/\ell$, where ℓ is the characteristic length, for example, the channel height, and obtained in the following form (note that superscript * is dropped from the equations):

$$u_{s} = \frac{2 - F_{m}}{F_{m}} Kn \left[\left(\frac{\mathrm{d}u}{\mathrm{d}\eta} \right)_{0} + Kn \left(\frac{\mathrm{d}^{2}u}{\mathrm{d}\eta^{2}} \right)_{0} + \frac{Kn^{2}}{2} \left(\frac{\mathrm{d}^{3}u}{\mathrm{d}\eta^{3}} \right)_{0} + \frac{Kn^{3}}{6} \left(\frac{\mathrm{d}^{4}u}{\mathrm{d}\eta^{4}} \right)_{0} + \cdots \right]$$

$$(7)$$

Further rearrangement of the terms results in

$$u_{s} = \frac{2 - F_{m}}{F_{m}} Kn \left(\frac{du}{d\eta}\right)_{0} \left\{ 1 + Kn \left[\frac{(d^{2}u/d\eta^{2})_{0}}{(du/d\eta)_{0}} \right] + \frac{Kn^{2}}{2} \left[\frac{(d^{3}u/d\eta^{3})_{0}}{(du/d\eta)_{0}} \right] + \frac{Kn^{3}}{6} \left[\frac{(d^{4}u/d\eta^{4})_{0}}{(du/d\eta)_{0}} \right] + \cdots \right\}$$
(8)

Next, we introduce the asymptotic expansion

$$1 / \left[1 - Kn \left(\frac{\mathrm{d}^2 u / \mathrm{d}\eta^2}{\mathrm{d}u / \mathrm{d}\eta} \right)_0 \right] = 1 + Kn \left(\frac{\mathrm{d}^2 u / \mathrm{d}\eta^2}{\mathrm{d}u / \mathrm{d}\eta} \right)_0$$
$$+ Kn^2 \left(\frac{\mathrm{d}^2 u / \mathrm{d}\eta^2}{\mathrm{d}u / \mathrm{d}\eta} \right)_0^2 + Kn^3 \left(\frac{\mathrm{d}^2 u / \mathrm{d}\eta^2}{\mathrm{d}u / \mathrm{d}\eta} \right)_0^3 + \cdots$$
(9)

to Eq. (8) and organize the resulting expression as

$$u_{s} = \frac{2 - F_{m}}{F_{m}} Kn \left(\frac{\mathrm{d}u}{\mathrm{d}\eta}\right)_{0} \left[1 / \left[1 - Kn \left(\frac{\mathrm{d}^{2}u/\mathrm{d}\eta^{2}}{\mathrm{d}u/\mathrm{d}\eta}\right)_{0}\right] + \frac{Kn^{2}}{2} \left(\frac{\mathrm{d}^{3}u/\mathrm{d}\eta^{3}}{\mathrm{d}u/\mathrm{d}\eta}\right)_{0} + \frac{Kn^{3}}{6} \left(\frac{\mathrm{d}^{4}u/\mathrm{d}\eta^{4}}{\mathrm{d}u/\mathrm{d}\eta}\right)_{0} + \cdots - \left(Kn \frac{\mathrm{d}^{2}u/\mathrm{d}\eta^{2}}{\mathrm{d}u/\mathrm{d}\eta}\right)_{0}^{2} - \left(Kn \frac{\mathrm{d}^{2}u/\mathrm{d}\eta^{2}}{\mathrm{d}u/\mathrm{d}\eta}\right)_{0}^{3} - \left(Kn \frac{\mathrm{d}^{2}u/\mathrm{d}\eta^{2}}{\mathrm{d}u/\mathrm{d}\eta}\right)_{0}^{3} - (Kn \frac{\mathrm{d}^{2}u/\mathrm{d}\eta^{2}}{\mathrm{d}u/\mathrm{d}\eta}\right)_{0}^{4} - \cdots \right]$$

$$(10)$$

or simply

(5)

$$u_s = \frac{2 - F_m}{F_m} \frac{Kn}{1 - bKn} \left(\frac{\mathrm{d}u}{\mathrm{d}\eta}\right)_0 + \text{res}$$
 (11)

where $b = (d^2u/d\eta^2)/(du/d\eta)$ and the residual is given by

$$\operatorname{res} = \frac{2 - F_m}{F_m} \left[\frac{Kn^3}{2} \left(\frac{d^3 u}{d\eta^3} \right)_0 + \frac{Kn^4}{6} \left(\frac{d^4 u}{d\eta^4} \right)_0 + \frac{Kn^5}{24} \left(\frac{d^5 u}{d\eta^5} \right)_0 + \cdots \right.$$

$$\left. - Kn^3 \frac{(d^2 u/d\eta^2)_0^2}{(du/d\eta)_0} - Kn^4 \frac{(d^2 u/d\eta^2)_0^3}{(du/d\eta)_0^2} \right.$$

$$\left. - Kn^5 \frac{(d^2 u/d\eta^2)_0^4}{(du/d\eta)^3} - \cdots \right]$$

$$\left. (12)$$

For flow between two parallel plates, we have $d^2u/d\eta^2 = -2$ and $du/d\eta = 1$. Therefore, the coefficient b is calculated to be equal to -2. The analysis of Ref. 4 using the velocity boundary condition obtained b = -1. The velocity boundary condition was first introduced by Schaaf and Chambre.⁵ They took the slip velocity as the average of the tangential velocity of the approaching and the reflected molecules. They assumed that the velocity of approaching molecules is the same as the velocity on the Knudsen layer and, therefore, is the velocity of the specularly reflected molecules. They obtained the slip velocity as

$$u_s = \frac{1}{2}(u_{\text{in}} + u_{\text{out}}) = \frac{1}{2}[u_{\lambda} + (1 - F_m)u_{\lambda}] = [(2 - F_m)/2]u_{\lambda}$$
 (13)

The velocity at $y = \lambda$ was written by expanding the velocity profile around y = 0. Beskok and Karniadakis⁴ used the first two terms of this expansion and obtained the second-order slip boundary condition without the residual term with $b = \frac{1}{2}(d^2u^*/d\eta^2)_0/(du^*/d\eta)_0$.

Figure 3 shows the slip velocity for three different analyses for $10^{-2} \le Kn \le 2$. The dashed line corresponds Beskok and Karniadakis's velocity boundary condition⁴ and the solid line corresponds to the present stress boundary condition. The stress boundary condition provides better results than the velocity boundary condition compared to the linearized Boltzmann solution of Ohwada et al.⁶

Note that the resultant stress boundary condition can be used for only small Knudsen number Kn values, where the characteristic length is larger than the Knudsen layer. In addition to this physical limit, a mathematical lower limit is also introduced by the given asymptotic expansion. Assuming a parabolic velocity profile and using the values of the first- and second-order derivatives at the wall, we can write the residual as

res =
$$-\sum_{i=2}^{\infty} K n^{i+1} (-2)^i$$

The residual is calculated for different values of Knudsen number Kn, and the resulting error values with respect to the calculated slip velocity are shown in Table 1. Negative values of the residual explain

Table 1 Error generated from asymptotic expansion

Kn	Residual	\mathbf{u}_s	% Error
0.0	0.0	0.0	0.0
0.1	-0.0033	0.3333	0.99
0.2	-0.0229	0.4615	4.9
0.3	-0.0675	0.5294	12.7
0.4	-0.1422	0.5714	24.88
0.5	0.0	0.6	0.0
0.6	-3.25×10^{7}	0.6207	∞

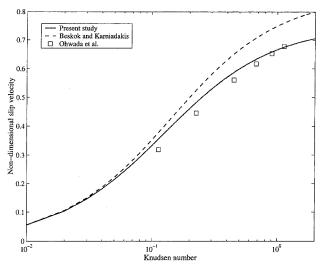


Fig. 3 Comparison of the slip velocity in $10^{-2} \le Kn \le 2$.

the overestimation of the slip velocity as shown in Fig. 3. Based on the error analysis, we can conclude that our approximation is valid up to Knudsen numbers around 0.5. This conclusion is consistent with the physical constraint of Kn < 1.

A similar boundary condition for a cylindrical pipe will now be derived. The velocity λ away from the surface is obtained as

$$u_{R-\lambda} = -\frac{2 - F_m}{F_m} \lambda \left(\frac{\mathrm{d}u}{\mathrm{d}y}\right)_{R-\lambda} \tag{14}$$

We expand the derivative around r = R, where R is the channel radius:

$$\left(\frac{\mathrm{d}u}{\mathrm{d}y}\right)_{R-\lambda} = \left(\frac{\mathrm{d}u}{\mathrm{d}y}\right)_{R} - \lambda \left(\frac{\mathrm{d}^{2}u}{\mathrm{d}y^{2}}\right)_{R} + \frac{\lambda^{2}}{2} \left(\frac{\mathrm{d}^{3}u}{\mathrm{d}y^{3}}\right)_{R} + \cdots$$
 (15)

Equation (15) is substituted into Eq. (14), and the following expansion is utilized:

$$1 / \left(1 + Kn \frac{\mathrm{d}^2 u / \mathrm{d}\eta^2}{\mathrm{d}u / \mathrm{d}\eta} \right) = 1 - Kn \frac{\mathrm{d}^2 u / \mathrm{d}\eta^2}{\mathrm{d}u / \mathrm{d}\eta} + Kn^2 \left(\frac{\mathrm{d}^2 u / \mathrm{d}\eta^2}{\mathrm{d}u / \mathrm{d}\eta} \right)^2 - Kn^3 \left(\frac{\mathrm{d}^2 u / \mathrm{d}\eta^2}{\mathrm{d}u / \mathrm{d}\eta} \right)^3 + \cdots$$
(16)

to obtain

$$u_{s}^{*} = -\frac{2 - F_{m}}{F_{m}} \frac{Kn}{1 + bKn} \left(\frac{\mathrm{d}u^{*}}{\mathrm{d}\eta}\right)_{n=1}$$
 (17)

where

$$u^* = \frac{u}{u_m}, \qquad \eta = \frac{y}{R}, \qquad b = \frac{(d^2 u^* / d\eta^2)_{\eta = 1}}{(du^* / d\eta)_{\eta = 1}}, \qquad Kn = \frac{\lambda}{R}$$

The coefficient b is calculated as 1 for cylindrical geometry.

B. Temperature Jump

In this section, the derivation of temperature jump boundary condition as outlined by Kennard¹ will be presented. The derivation starts with the definition of the thermal accommodation coefficient as $F_T = (Q_i - Q_r)/(Q_i - Q_w)$. Q_i is the energy of the impinging molecules, Q_r is the energy carried by the reflected molecules, and Q_w is energy that the molecules would have if they left the wall at the wall temperature.

The numerator of this relation is the net heat transfer and is given by

$$Q_i - Q_r = k \left(\frac{\partial T}{\partial y}\right)_{\lambda} \tag{18}$$

and the denominator is obtained from

$$Q_i - Q_{\lambda} = m \left(c_v + \frac{1}{2} R \right) (T_s - T_{\lambda}) + \frac{1}{2} k \left(\frac{\partial T}{\partial y} \right)_{\lambda}$$
 (19)

where the difference between the internal and kinetic energies of the approaching and reflected molecules is added to the heat conduction by the approaching molecules. In Eq. (19), m is the mass, c_v is the specific heat at constant volume, R is the gas constant, and k is the thermal conductivity. When the definition of F_T is used and the kinetic theory of gases is utilized, the temperature jump can be solved as

$$T_{\lambda} - T_{w} = \frac{2 - F_{T}}{F_{T}} \frac{2\gamma}{\gamma + 1} \frac{\lambda}{Pr} \left(\frac{\partial T}{\partial y}\right)_{\lambda}$$
 (20)

where γ is the specific heat ratio. Equation (20) provides the first-order boundary condition if the temperature gradient at the wall is assumed to be the same as the one on $y = \lambda$. The second-order temperature jump boundary condition is obtained by following the approach applied in obtaining the velocity slip boundary condition as

$$\theta_s - \theta_w = \frac{2 - F_T}{F_T} \frac{2\gamma}{\gamma + 1} \frac{Kn}{Pr(1 - aKn)} \left(\frac{\partial \theta}{\partial n}\right) \tag{21}$$

where Pr is the Prandtl number, θ is the nondimensional temperature, $\theta = T/T_{\text{reference}}$, subscripts s and w correspond to the fluid temperature at the wall and the wall temperature, and $a = (\mathrm{d}^2\theta/\mathrm{d}\eta^2)_0/(\mathrm{d}\theta/\mathrm{d}\eta)_0$.

Conclusions

The velocity slip and temperature jump boundary conditions were derived for $Kn \le 0.5$. Velocity gradient on the wall was obtained from the expansion of the gradient on Knudsen layer unlike the previous analyses that used the expansion of velocity itself. The slip velocities calculated from the present stress boundary condition agreed well with the linearized Boltzmann results.

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Transient Coupled Radiation and Conduction in a Two-Layer Semitransparent Material

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Introduction

S EMITRANSPARENT material (STM), in which the nature of the radiative transfer can provide a positive or negative internal heat source, is widely applied to engineering. Recently, some researchers have focused on coupled radiation and conduction in a two-layer or multilayer planer STM, such as Ho and Özisik, Spuckler and Siegel, and Siegel. The ray tracing/nodal analysis method was provided in Refs. 4 and 5 to obtain transient temperatures in a single-layer nonscattering STM and isotropically scattering STM, respectively. After that, Refs. 6 and 7 extended this

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method to a two-layer, isotropically scattering STM with the semitransparent or the opaque boundaries, respectively. Some conclusions were drawn, for example, when one side is heated and the other is cooled, the temperature maximums can appear inside the composite with both semitransparentboundaries⁶; however, for both opaque boundaries the temperature maximums only appear at the heated boundary.⁷ The derivation of this method is extended here for a two-layer, isotropically scattering and nongray composite with one semitransparent boundary and one opaque boundary, and the emphasis is placed on investigating whether the peak value of temperature will appearinside the composite and the effects of refractive index and conduction-radiation parameter on temperature distribution. The nomenclature used herein is the same as that of Refs. 6 and 7.

Analysis

A two-layer planar STM with one semitransparent boundary S_1 and one opaque boundary S_2 , as shown in Fig. 1, is located between two black surfaces $S_{-\infty}$ and $S_{+\infty}$, which, respectively, denote the outside surroundings. The reflectivities of surfaces S_1 , S_P , and S_2 are ρ_1 , ρ_P , and ρ_2 ; the transmissivities of semitransparent surfaces S_1 and S_P are γ_1 and γ_P . The composite is divided into M control volumes. For this physical model the energy equation and the radiative heat source for the transient coupled radiation and conduction are the same as those in Ref. 5, but the radiative transfer coefficient (RTC) and the boundary conditions need to be rededuced. The RTC is defined as the total quotient of the radiative energy arriving at the investigated element in the transfer process and the radiative energy emitted by another one. The transfer process of radiative energy in a scattering STM can be divided into two subprocesses: a nonscattering subprocess and a scattering subprocess. 5 The derivation of scattering subprocess⁵ is not provided here because it is independent of the radiative properties of the boundary surfaces. The notation for RTC given in Refs. 6 and 7 is still used, that is, $(S_u S_v)_k$, $(S_u V_j)_k$, and $(V_i V_j)_k$ denote RTCs of surface S_u transferring to surface S_v , surface S_u transferring to volume V_j , and volume V_i transferring to volume V_i for nonscattering materials, respectively; and $[S_u S_v]_k$, $[S_u V_j]_k$, and $[V_i V_j]_k$ denote RTCs for scattering materials. S_u and S_v denote surface $S_{-\infty}$ or S_2 ; V_i and V_j denote the *i*th and *j*th control volumes, respectively; and subscript k refers to the spectral band of interest.

Radiative Transfer Coefficient

Take $(S_{-\infty}V_j)_k$ as an example and assume that V_j belongs to the second layer. The deductive process used in determining the RTCs for diffuse reflection are provided here through tracing the radiative energy by using the philosophy of the ray tracing method in combination with the direct radiative transfer coefficient (DRTC). The DRTC is defined as the RTC not considering reflection and is denoted by $(s_w s_z)_k$, $(s_w v_j)_k$, and $(v_i v_j)_k$, whose equations are given in Ref. 7; s_w and s_z denote surfaces S_1 , S_P , or S_2 ; and v_i and v_j denote control volumes V_i and V_j , respectively.

For the unit radiative energy that comes from $S_{-\infty}$, a part entering the composite through surface S_1 is absorbed by the first layer medium, then transmitted and reflected through surfaces S_1 and S_P . In the end it is attenuated to zero. In this transfer process

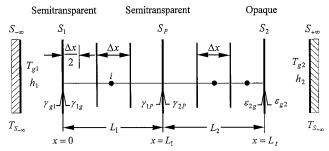


Fig. 1 Zonal discretization model of a two-layer planar composite medium.

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